

# Numerical study of the fluid flow and interface deflection for crystals grown by Bridgman technique

Simina Maris and Liliana Braescu

**Abstract**—A stationary, free boundary model describing the process of crystal growth in a vertical Bridgman installation is considered. For this model, the influence of the temperature profile in the furnace and gravitational field on the fluid flow and interface deflection, are investigated numerically by finite element method through FreeFem++ software.

**Index Terms**—Free boundary problem, Stationary problem, Temperature profile, Interface deflection, Vertical Bridgman, Gravitational field, Numerical simulation

## I. INTRODUCTION

The Bridgman technique is a popular method of growing single crystals from compound materials that contain a volatile element. This is the case of the entire group III-V and II-VI semiconductor crystals. The method consists in movement of a crucible (ampoule), charged with powder and a seed, through a temperature gradient. The ampoule is introduced in the hot region of the furnace until the powder is melted, and then it is pulled with a rate  $\bar{u}_{translation}$ , such that it enters into the cold region and the solidification process begins [1].

The factors that influence the quality of the resulting crystal are:

- the temperature gradient in the furnace;
- the gravitational field;
- the properties of the material (e.g., specific heat, density, kinematic viscosity, thermal expansion coefficient, solidification temperature, initial dopant concentration);
- the ampoules velocity of translation in the furnace;
- the shape of solid-melt interface.

In the case of alloys for which equilibrium segregation coefficient of the dopant is less than unity, a serious problem is the amount of dopant rejected at the solid-melt interface. This quantity depends on the velocity field in melt and on the shape of solidification interface. Both these parameters depend on the value of the gravitational field and on the temperature profile inside the furnace.

In literature, there are several numerical investigations of the solidification process in vertical Bridgman installations ([2]-[11]).

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In this paper, the dependence of fluid flow and interface deflection on the temperature profile are investigated numerically in a vertical Bridgman furnace, for various values of the gravitational field. The numerical simulations, based on a fixed-point algorithm, were performed using the FreeFem++ software.

## II. MATHEMATICAL FORMULATION

Let us consider the stationary, free boundary model proposed in [3]. Because the crucible presents axial symmetry, the three-dimensional problem could be reduced to a two-dimensional one. Denoting by  $\Omega_l$  the domain occupied by melt,  $\Omega_s$  the domain occupied by crystal and the solidification interface by a function  $h(r)$ , we have [9]:

$$\Omega_s = \{(r, z) \in \mathbb{R}^2 \mid 0 < r < R \text{ and } 0 < z < h(r)\}$$

$$\Omega_l = \{(r, z) \in \mathbb{R}^2 \mid 0 < r < R \text{ and } h(r) < z < A\}$$

$$h(R) = \frac{A}{2}$$

A schematic representation of the computational domains is given in Figure 1, where  $A = 1$  represents the dimensionless length of the ampoule,  $R = 0.25$  is the dimensionless radius of the ampoule and  $L_g$  is the length of the gradient zone.

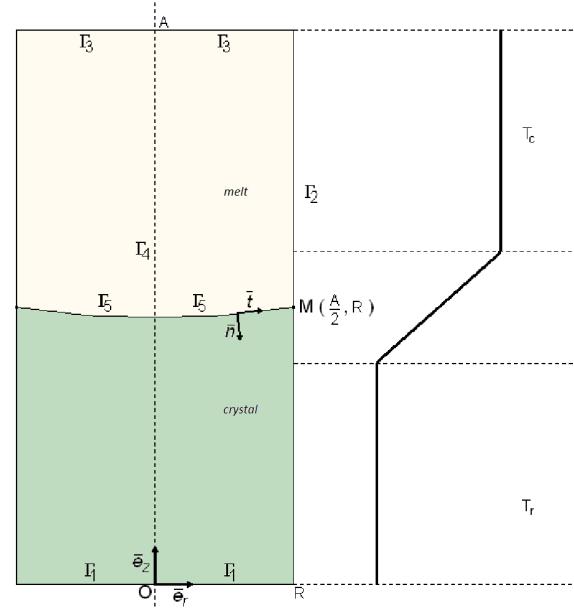


Fig. 1. The computational domains and the temperature profile inside the furnace

The translation of the ampoule inside the furnace is simulated by adding melt at  $z = A$  and pulling crystal at  $z = 0$ .

The dimensionless equations governing the process are

$$\left\{ \begin{array}{l} \bar{u} = 0 \text{ in } \Omega_l \\ (\bar{u} \nabla) \bar{u} = -\nabla p + Pr \Delta \bar{u} + Ra Pr \theta \bar{k} \text{ in } \Omega_l \\ \bar{u} \nabla \theta = \Delta \theta \text{ in } \Omega_l \\ \bar{u}_c = -Pe \bar{k} \text{ in } \Omega_s \\ \bar{u}_c \nabla \theta_c = \gamma \Delta \theta_c \text{ in } \Omega_s \end{array} \right. \quad (1)$$

where  $\bar{u}$  represents the dimensionless velocity of the melt;  $\bar{u}_c$  - the dimensionless velocity of the crystal;  $\theta$  - the dimensionless temperature of the melt;  $\theta_c$  - the dimensionless temperature of the crystal;  $Ra$  (thermal Rayleigh number) defines the gravitational field ( $Ra = 0$  for zero gravity,  $Ra = 10^3$  for micro-gravity,  $Ra = 10^6$  for normal gravity);  $Pr = 0.01$  (Prandtl number) represents the dimensionless kinematic viscosity;  $Pe = 0.01$  (Peclet number) represents the dimensionless translation velocity of the ampoule inside the furnace;  $\gamma = 1$  is the ratio of solid and melt thermal diffusivities.

The boundary conditions are:

$$\bar{u}|_{\Gamma_2, \Gamma_3} = \bar{u}_{tr} \quad (2)$$

$$\bar{u}_c|_{\Gamma_1, \Gamma_2} = \bar{u}_{tr} \quad (3)$$

$$\bar{u} \cdot \bar{t}|_{\Gamma_5} = Pe \cdot t_z \quad (4)$$

$$\sigma(\bar{u} \cdot \bar{n})|_{\Gamma_5} = Pe \cdot n_z \quad (5)$$

$$\theta_c|_{\Gamma_1} = 0 \quad (6)$$

$$\theta|_{\Gamma_2} = \begin{cases} \frac{1}{L_g}z + \frac{L_g - A}{2L_g}, & z \in \left[\frac{A}{2}, \frac{A}{2} + \frac{L_g}{2}\right] \\ 1, & z > \frac{A}{2} + \frac{L_g}{2} \end{cases} \quad \text{not } = \tau \quad (7)$$

$$\theta_c|_{\Gamma_2} = \begin{cases} 0, & z < \frac{A}{2} - \frac{L_g}{2} \\ \frac{1}{L_g}z + \frac{L_g - A}{2L_g}, & z \in \left[\frac{A}{2} - \frac{L_g}{2}, \frac{A}{2}\right] \end{cases} \quad \text{not } = \tau_c \quad (8)$$

$$\theta|_{\Gamma_3} = 1 \quad (9)$$

$$\theta|_{\Gamma_5} = \theta_c|_{\Gamma_5} = 0.5 \quad (10)$$

$$[(\bar{n} \nabla \theta)_l - k (\bar{n} \nabla \theta)_s]|_{\Gamma_5} = S Pe n_z \quad (11)$$

where  $\bar{u}_{tr} = -0.01\bar{e}_z$  is the dimensionless velocity of translation of ampoule.

### III. NUMERICAL STUDY OF THE FLUID FLOW AND INTERFACE DEFLECTION

The numerical simulations were performed using FreeFem++, software developed at Université Pierre et Marie Curie, Paris [12], dedicated to solve nonlinear two-dimensional and three-dimensional partial differential equations, using the finite element method.

As one can observe from equations (7)-(8), the temperature profile in the furnace is considered a linear function on  $z$ -coordinate and depends by the length of the gradient zone,  $L_g$ .

For investigating numerically the fluid flow and the shape of the fluid-melt interface, different values of  $L_g$  (from  $L_g = \frac{1}{8}A$  to  $L_g = A$ ) are considered, in the case of zero gravity, micro-gravity, respectively normal gravity conditions.

The free boundary is obtained from a fixed-point algorithm, presented in [10]. It takes as input data  $h^{(0)}(r) = \frac{A}{2}$ ,  $\bar{u}^{(0)}(r, z) = \bar{u}_{tr}$ ,  $\theta^{(0)}(r, z) = \tau$ ,  $\theta_c^{(0)}(r, z) = \tau_c$ , and computes  $h(r)$ ,  $\bar{u}(r, z)$ ,  $\theta(r, z)$ ,  $\theta_c(r, z)$ , as follows:

- 1) solve the heat equation with the boundary condition (11);
- 2) find the isotherm corresponding to (10);
- 3) construct a domain deformation in order to overlap the boundary to the isotherm found at the previous step;
- 4) solve the Navier-Stokes equation on the deformed domain;
- 5) repeat steps 1-4 until both variations of temperature field and velocity field become less than a sufficiently small value,  $\varepsilon$ .

#### A. Case of zero gravity

The zero gravity conditions ( $Ra = 0$ ) imply that the body forces in the Navier-Stokes equation are zero. As a consequence, the temperature profile in the furnace does not influence the velocity field in the melt. The streamlines of the computed velocity field and temperature profile for different values of  $L_g$  in absence of gravity are plotted in Figs. 2-7.

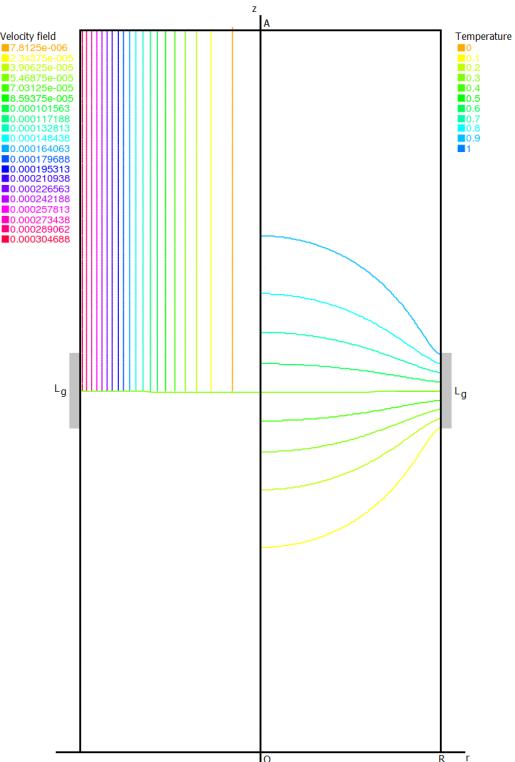
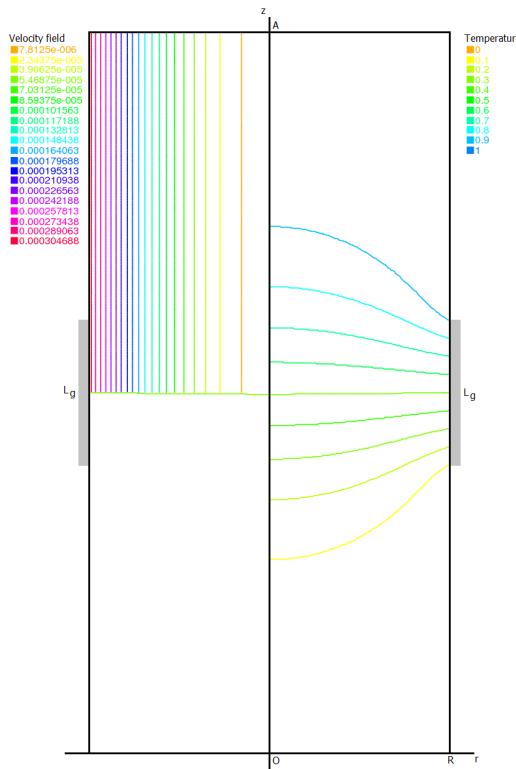
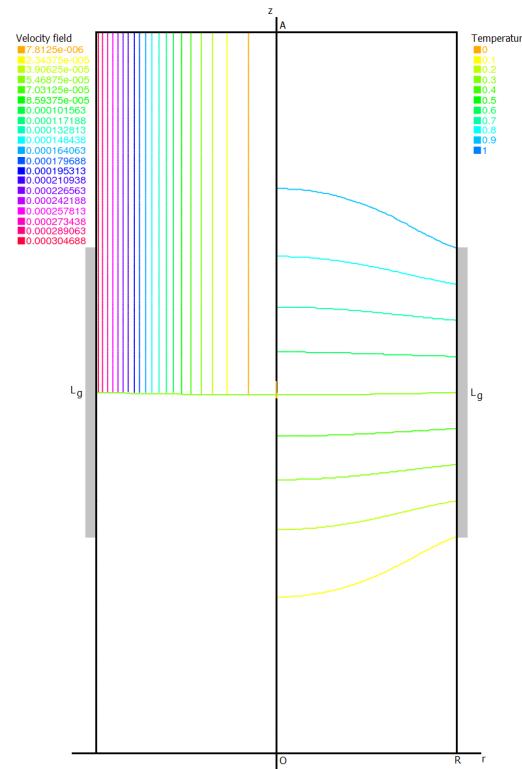
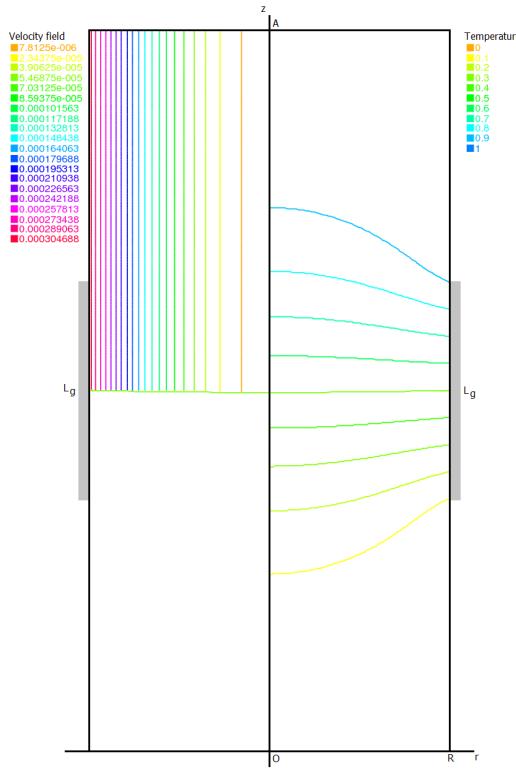
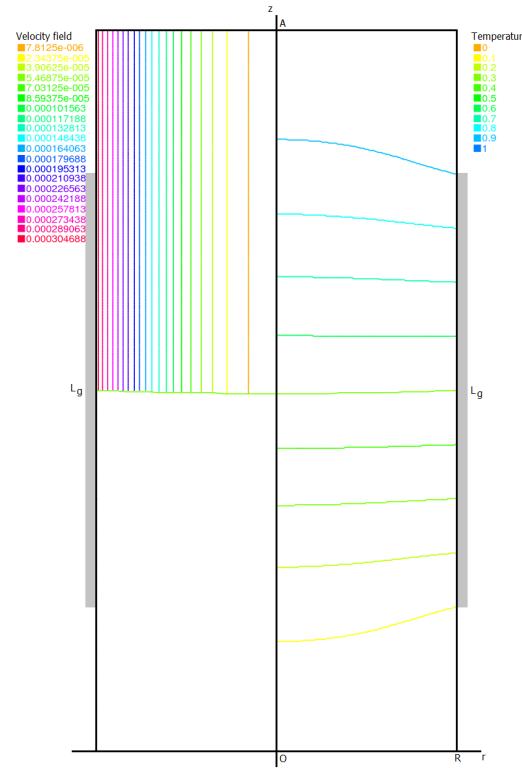


Fig. 2. Streamlines and temperature profile for  $L_g = 0.125$ ,  $Ra = 0$ .

Figures show that the velocity fields present no convection cell, the movement of the melt being only determined by the


 Fig. 3. Streamlines and temperature profile for  $L_g = 0.250$ ,  $Ra = 0$ .

 Fig. 5. Streamlines and temperature profile for  $L_g = 0.500$ ,  $Ra = 0$ .

 Fig. 4. Streamlines and temperature profile for  $L_g = 0.375$ ,  $Ra = 0$ .

 Fig. 6. Streamlines and temperature profile for  $L_g = 0.750$ ,  $Ra = 0$ .

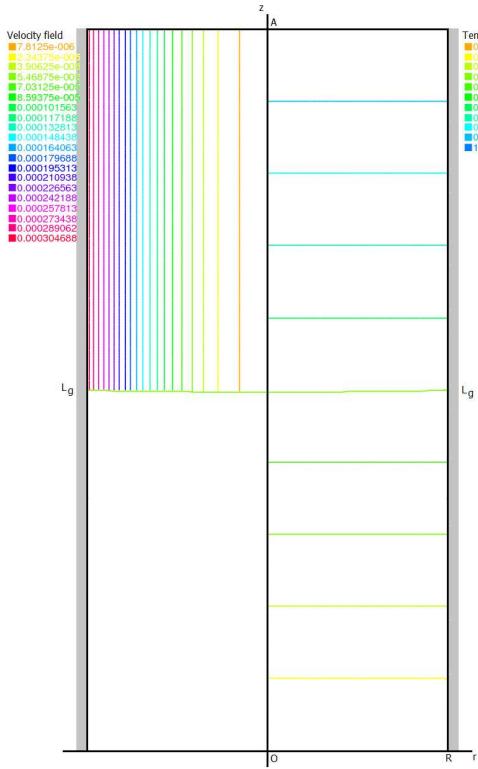


Fig. 7. Streamlines and temperature profile for  $L_g = 1.000$ ,  $Ra = 0$ .

TABLE I  
MAXIMUM VALUE OF THE STREAMLINES OF THE FLUID FLOW FOR DIFFERENT  $L_g$

$L_g$	$\Phi_{max}$ for $Ra = 0$
0.125	0.000304688
0.250	0.000304688
0.375	0.000304688
0.500	0.000304688
0.750	0.000304688
1.000	0.000304688

pulling rate,  $\bar{u}_{tr}$ . Also, the amplitude of the velocity field,  $\Phi_{max}$ , does not depend on the length of the gradient zone (see Table I).

The deflection of the interface in zero gravity for the considered  $L_g$  is presented in Figure 8. This figure shows that variations of  $L_g$  in the range [0.125, 1] produce small variations on the melt-solid interface. The solidification interface is a slight-convex shape and, for  $L_g = 1$ , it tends to be flatten.

### B. Case of micro-gravity

In micro-gravity conditions ( $Ra = 10^3$ ), the non-zero body forces in the Navier-Stokes equation determine a weak convection. Below, the computed streamlines in the melt and temperature inside the furnace obtained for different values of  $L_g$  in micro-gravity conditions are presented.

Figures 9-14 show that, in micro-gravity conditions, the velocity fields present a weak convection cell. Also, if the gradient zone increases from 0.125 to 1, then the streamlines

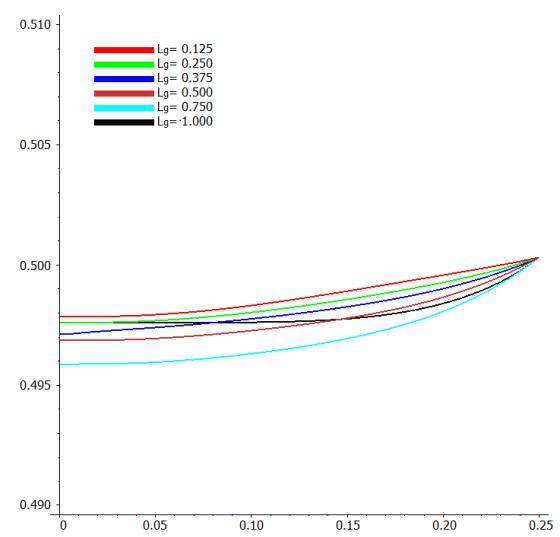


Fig. 8. The solidification interface corresponding to different values of  $L_g$ , for  $Ra = 0$

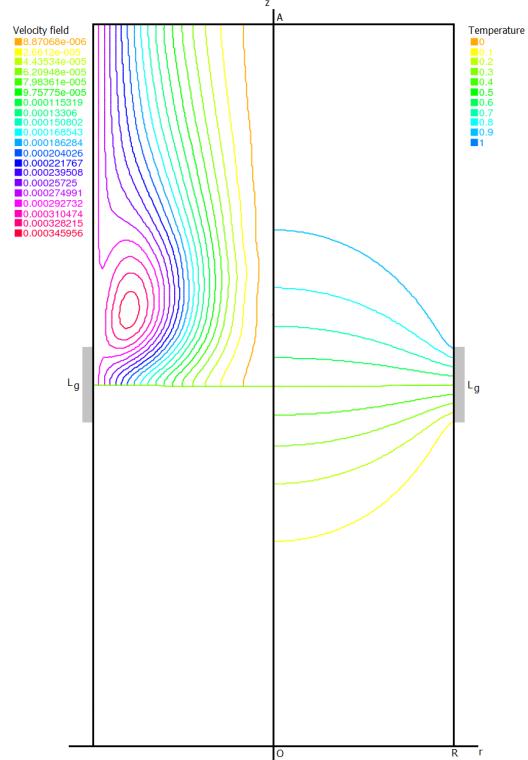


Fig. 9. Streamlines and temperature profile for  $L_g = 0.125$ ,  $Ra = 10^3$ .

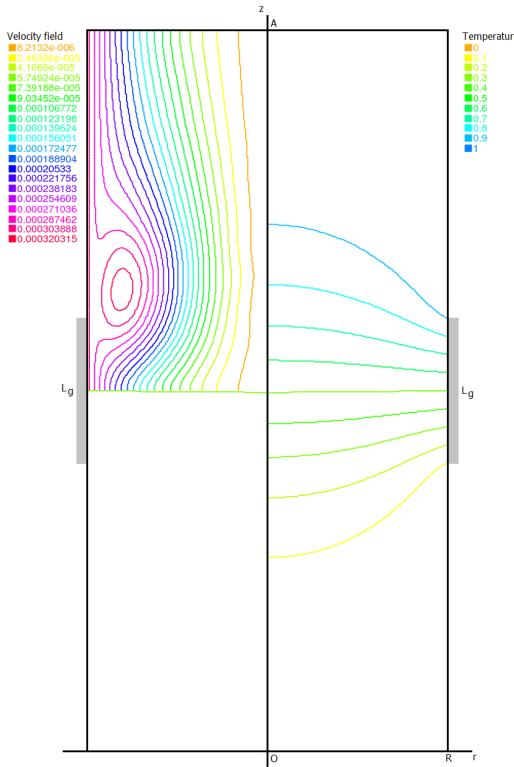


Fig. 10. Streamlines and temperature profile for  $L_g = 0.250$ ,  $Ra = 10^3$ .

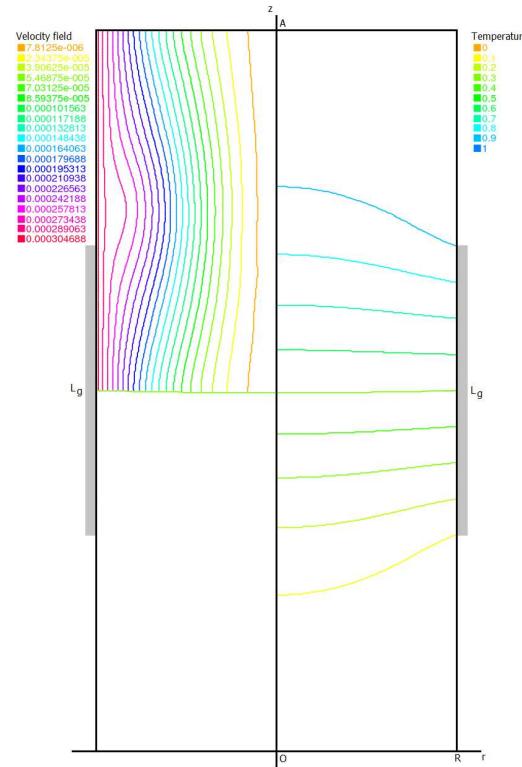


Fig. 12. Streamlines and temperature profile for  $L_g = 0.500$ ,  $Ra = 10^3$ .

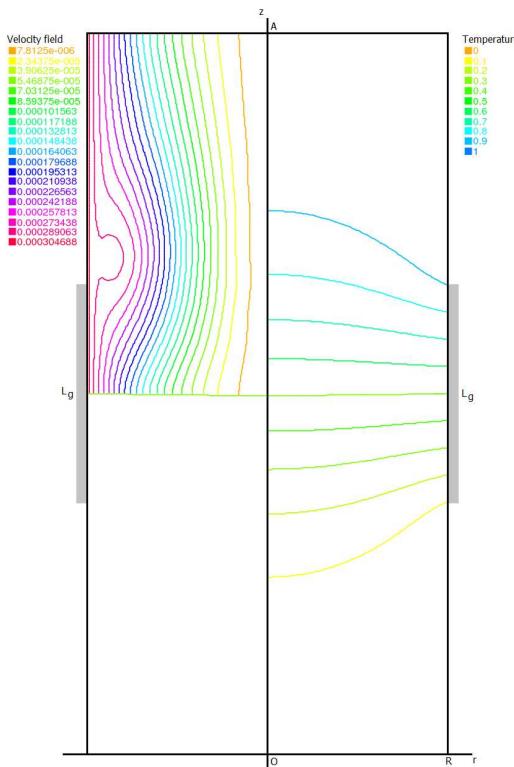


Fig. 11. Streamlines and temperature profile for  $L_g = 0.375$ ,  $Ra = 10^3$ .

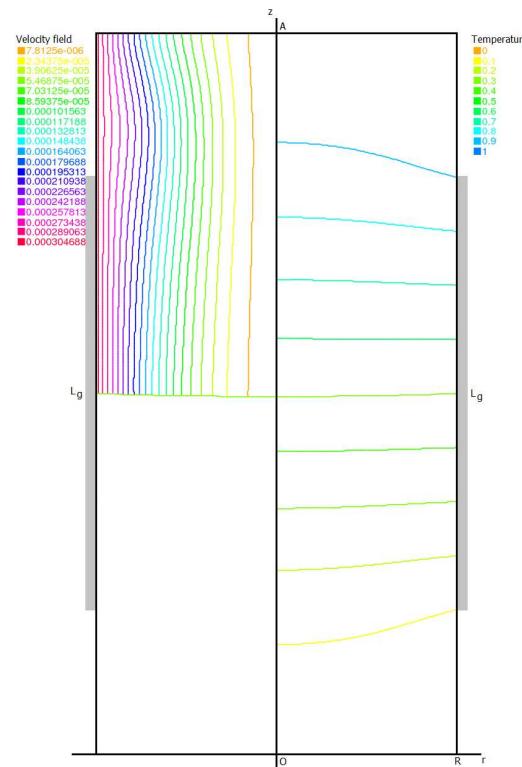


Fig. 13. Streamlines and temperature profile for  $L_g = 0.750$ ,  $Ra = 10^3$ .

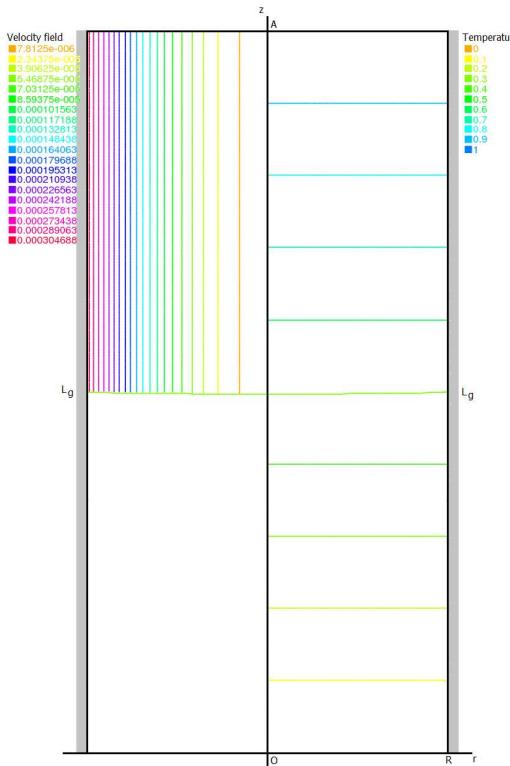
Fig. 14. Streamlines and temperature profile for  $L_g = 1.000$ ,  $Ra = 10^3$ .

TABLE II  
MAXIMUM VALUE OF THE STREAMLINES OF THE FLUID FLOW FOR  
DIFFERENT  $L_g$

$L_g$	$\Phi_{max}$ for $Ra = 10^3$
0.125	0.000345956
0.250	0.000320315
0.375	0.000304688
0.500	0.000304688
0.750	0.000304688
1.000	0.000304688

of the fluid flow have a maximum situated above the gradient zone. These maxima decrease as  $L_g$  increases (see Table II).

The deflection of the interface for the considered  $L_g$  (see Figure 15) shows that variations of  $L_g$  in the range [0.125, 1] produce small variations on the melt-solid interface, which preserve a slight-convex shape. If  $L_g = 1$ , then the interface shape tends to be flatten.

### C. Case of normal gravity

In normal gravity conditions ( $Ra = 10^6$ ), the body forces in the Navier-Stokes equation determine a strong convection. This alters both the shape of the velocity and temperature fields. The computed streamlines and temperature profiles, obtained for different values of the gradient zone length,  $L_g$ , are presented in Figs. 16-21.

Computations show that, in terrestrial gravity conditions, the velocity fields present a strong convection cell, which has a maximum situated above the gradient zone. These maxima decrease as  $L_g$  increases (see Table III).

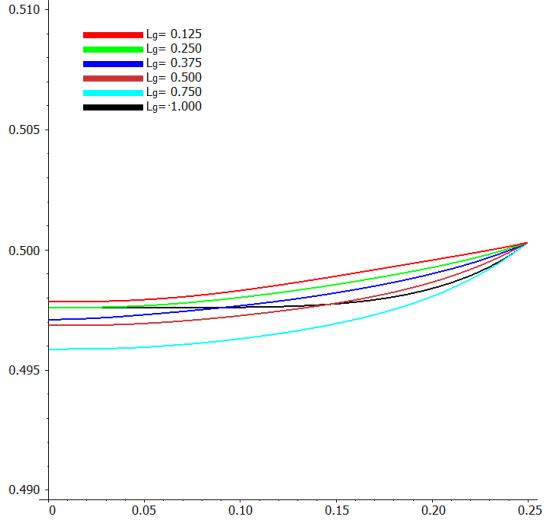
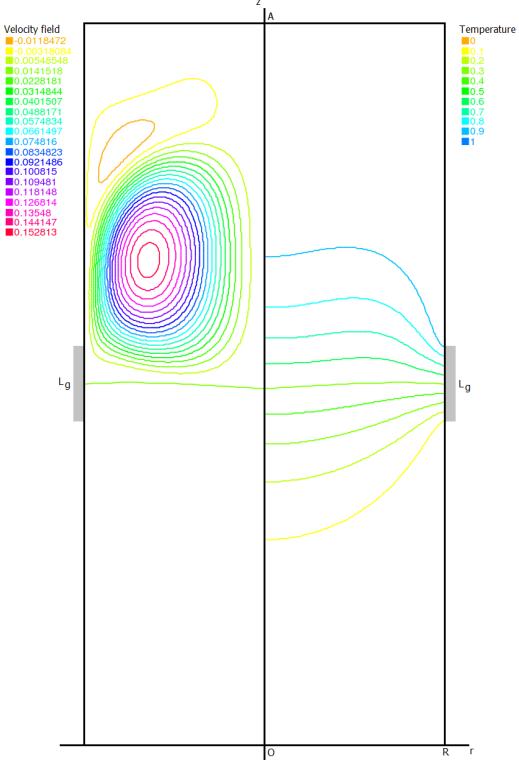
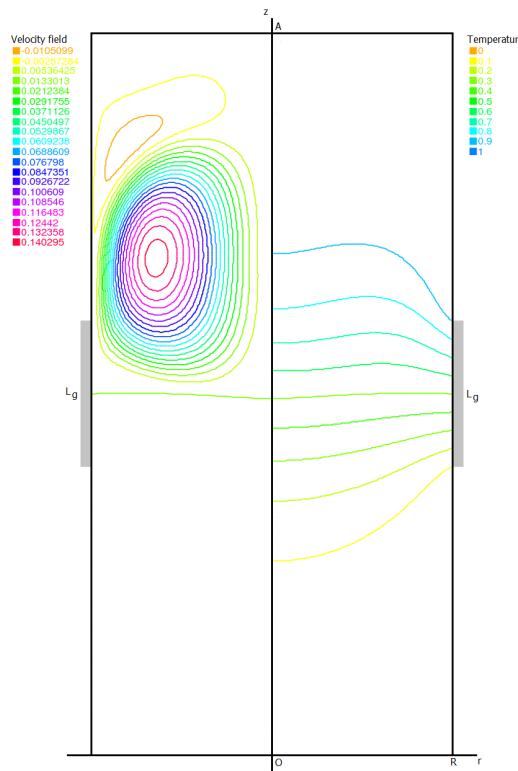
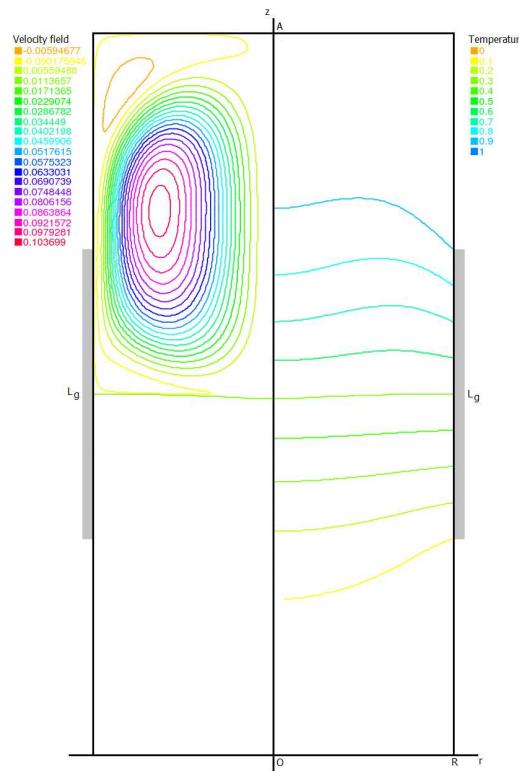
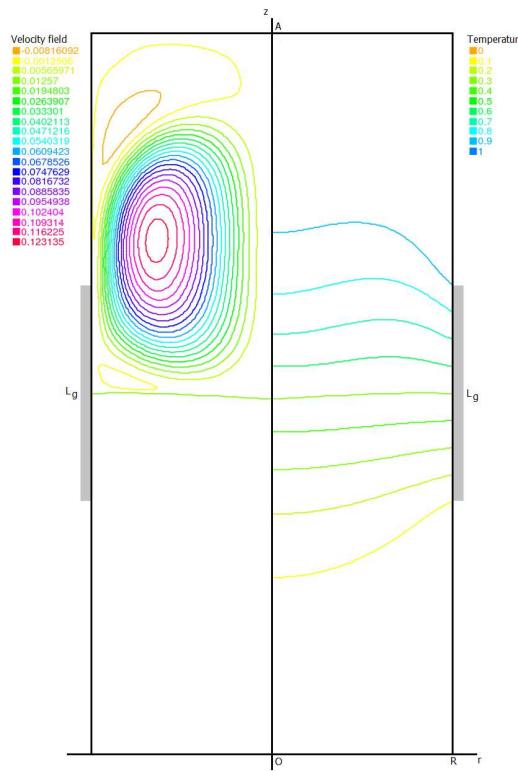
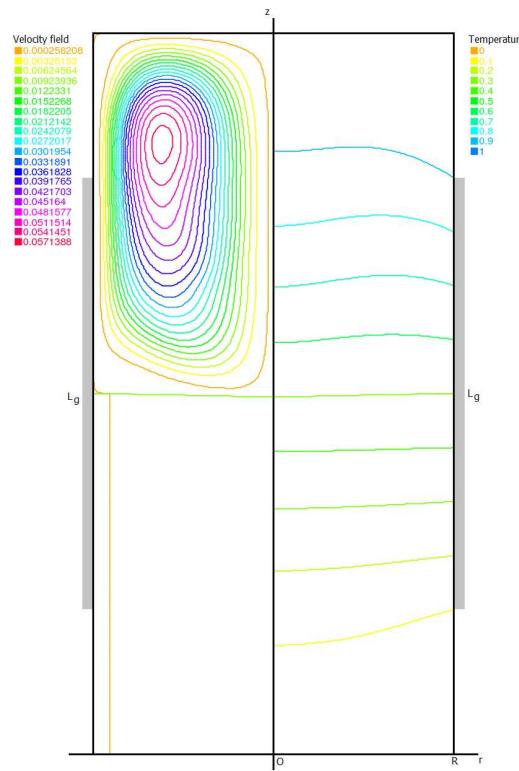
Fig. 15. The solidification interface corresponding to different values of  $L_g$  for  $Ra = 10^3$ Fig. 16. Streamlines and temperature profile for  $L_g = 0.125$ ,  $Ra = 10^6$ .

TABLE III  
MAXIMUM VALUE OF THE STREAMLINES OF THE FLUID FLOW FOR  
DIFFERENT  $L_g$

$L_g$	$\Phi_{max}$ for $Ra = 10^6$
0.125	0.152813
0.250	0.140295
0.375	0.123135
0.500	0.103699
0.750	0.0571388
1.000	0.000304688


 Fig. 17. Streamlines and temperature profile for  $L_g = 0.250$ ,  $Ra = 10^6$ .

 Fig. 19. Streamlines and temperature profile for  $L_g = 0.500$ ,  $Ra = 10^6$ .

 Fig. 18. Streamlines and temperature profile for  $L_g = 0.375$ ,  $Ra = 10^6$ .

 Fig. 20. Streamlines and temperature profile for  $L_g = 0.750$ ,  $Ra = 10^6$ .

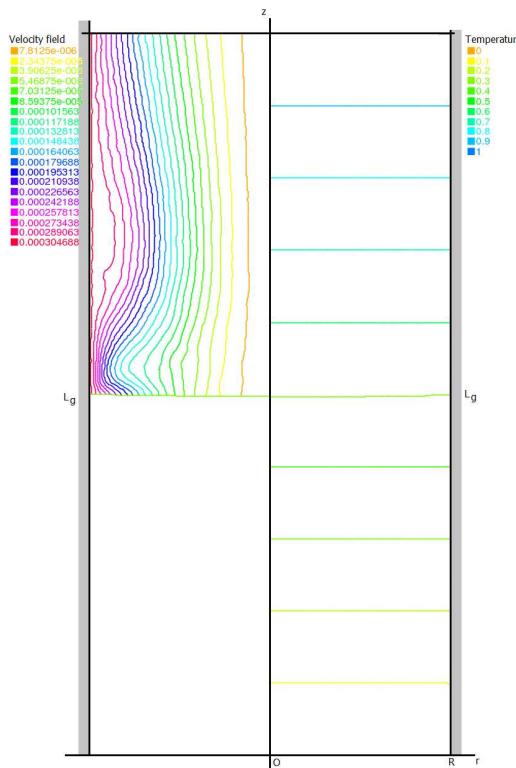


Fig. 21. Streamlines and temperature profile for  $L_g = 1.000$ ,  $Ra = 10^6$ .

The deflection of the interface for the considered  $L_g$  is presented in Figure 22. This figure shows that variations of

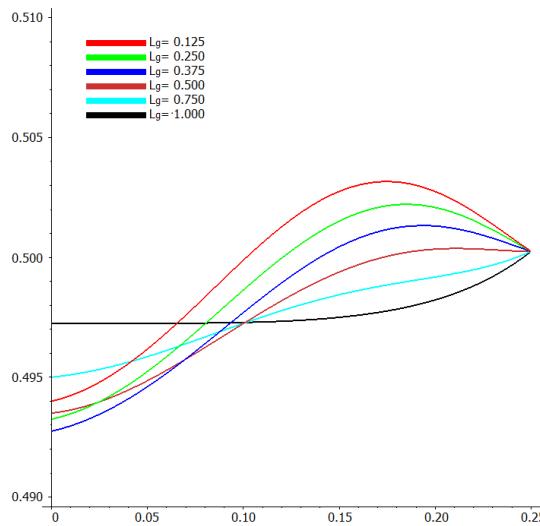


Fig. 22. The solidification interface corresponding to different values of  $L_g$

$L_g$  in the range  $[0.125, 0.500]$  produce small variations on the melt-solid interface, but deflection of the interface is quite large. If  $L_g$  increases to 1, then the interface deflection decreases. Also, the shape of the interface changes from "S"-shape to slight-convex shape when  $L_g$  increases and, for  $L_g = 1$ , the interface shape tends to be flatten.

#### IV. CONCLUSIONS

In this paper, the influence of the temperature profile in a vertical Bridgman installation on the fluid flow and interface deflection was studied. For all considered gravity conditions, it can be observed that the streamline amplitude decreases and the shape of the solidification interface tends to be flatten as the length of the gradient zone in the furnace increases to 1. Also, for a given length of the gradient zone,  $L_g$ , stronger gravitational forces tend to increase the amplitude of the streamlines and to flatten the isotherms in the melt. For  $L_g = 1$ , the gravitational field has no influence on the velocity field in the melt nor the temperature profile (and melt-solid interface) in the ampoule.

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